



LEAF RESOURCES LIMITED

Sustainable products from plant biomass

Glycell™ – Leaf Resources' pretreatment process for the conversion of lignocellulosic biomass to fuels and chemicals

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Forward Looking Statements



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Outline



- ▶ Glycell™ Cellulosic Sugars (CS) Process
 - ▶ Glycell at pilot scale
- ▶ Saccharification kinetics
- ▶ Cellulosic sugars production and fermentation tests
- ▶ Glycerol recovery by SMB chromatography
- ▶ Approaches to market
 - ▶ Pulp mill expansion, Retrofit, bolt-on, Greenfield
- ▶ Key technological advantages

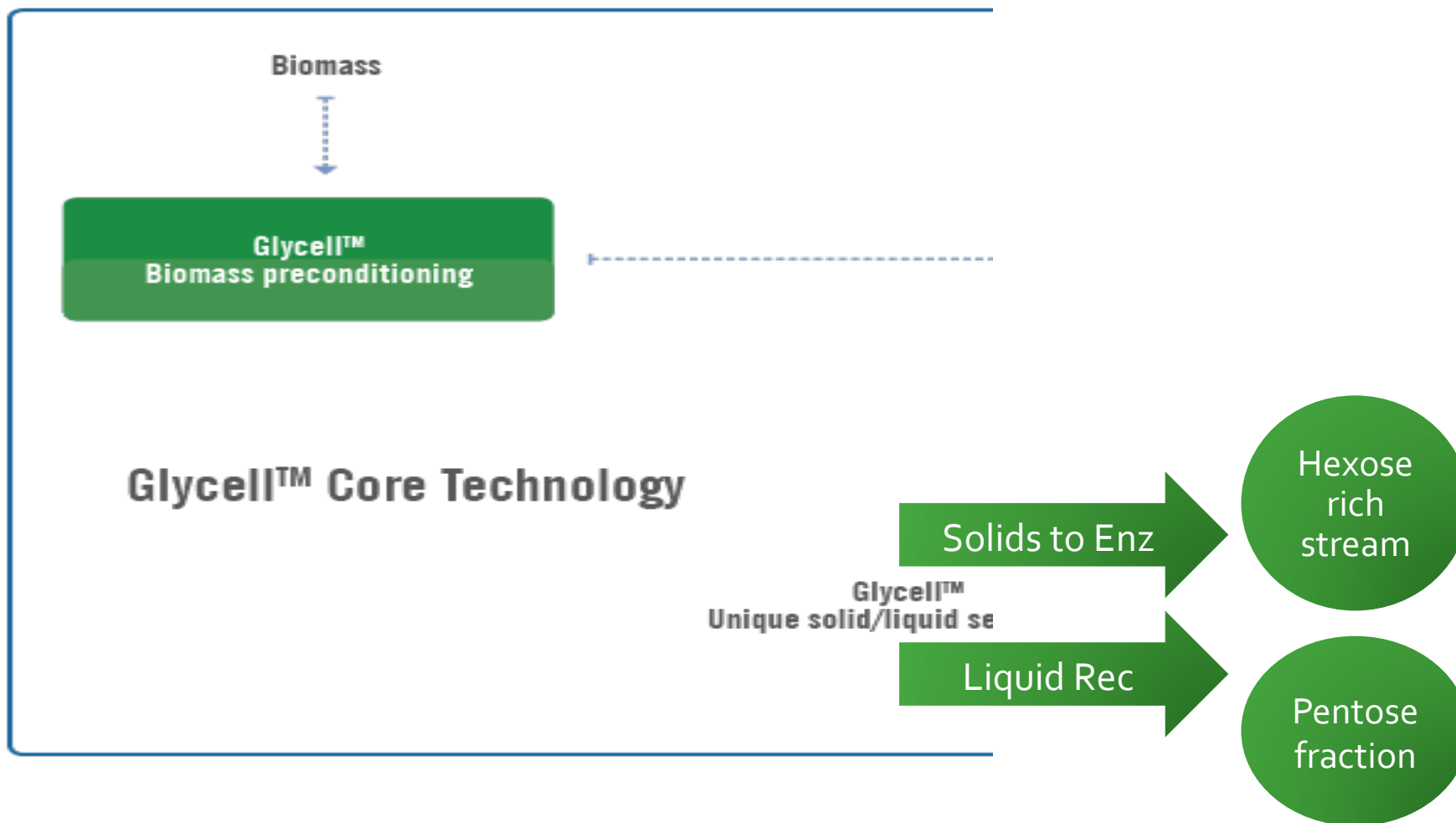
Leaf Resources

Active participants in the advanced bio-economy



- ▶ Leaf Resources Limited (ASX:LER) is focused on making sustainable products from plant biomass.
- ▶ We offer an advanced technology package for breaking down plant derived biomass to useful, sustainable, renewable and biodegradable products.
- ▶ Leaf Resources' innovative Glycell™ is a disruptive process technology that can reshape the economics of using large scale biomass resources as a replacement for petroleum derived products.

Leaf Resources Glycell™ CS Process



Glycell at pilot scale



- ▶ Several trials at the Andritz pilot plant facility in Springfield since November 2013
- ▶ Continuous production rates of 3-5 BDT per day
- ▶ > 40 independent pilot scale tests totalling over > 20 tonnes (dry basis) biomass
- ▶ Data presented here do not represent proprietary optimised conditions, but are chosen from pilot plant data to demonstrate the technical advantages of the Glycell process.

Biomass flexibility

Poplar



Oil Palm fibre (EFB)



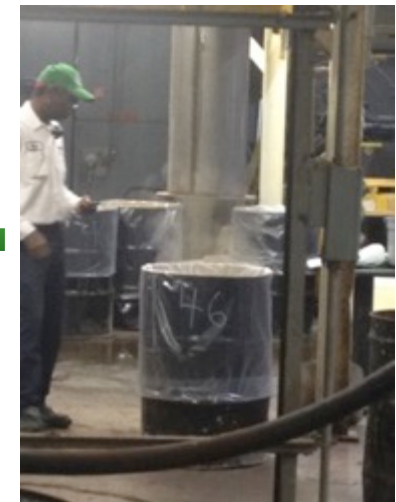
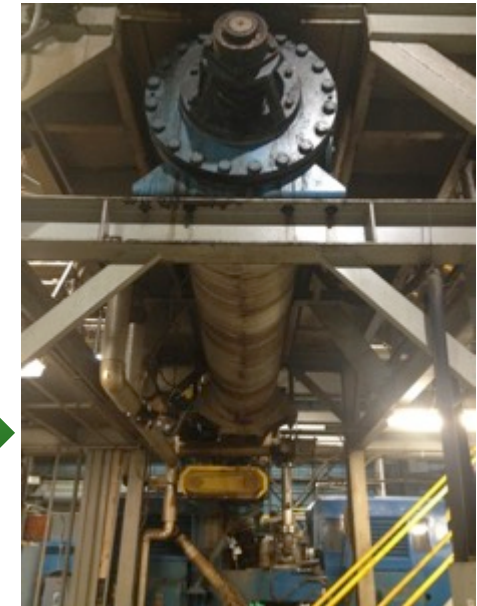
Bagasse



Eucalyptus

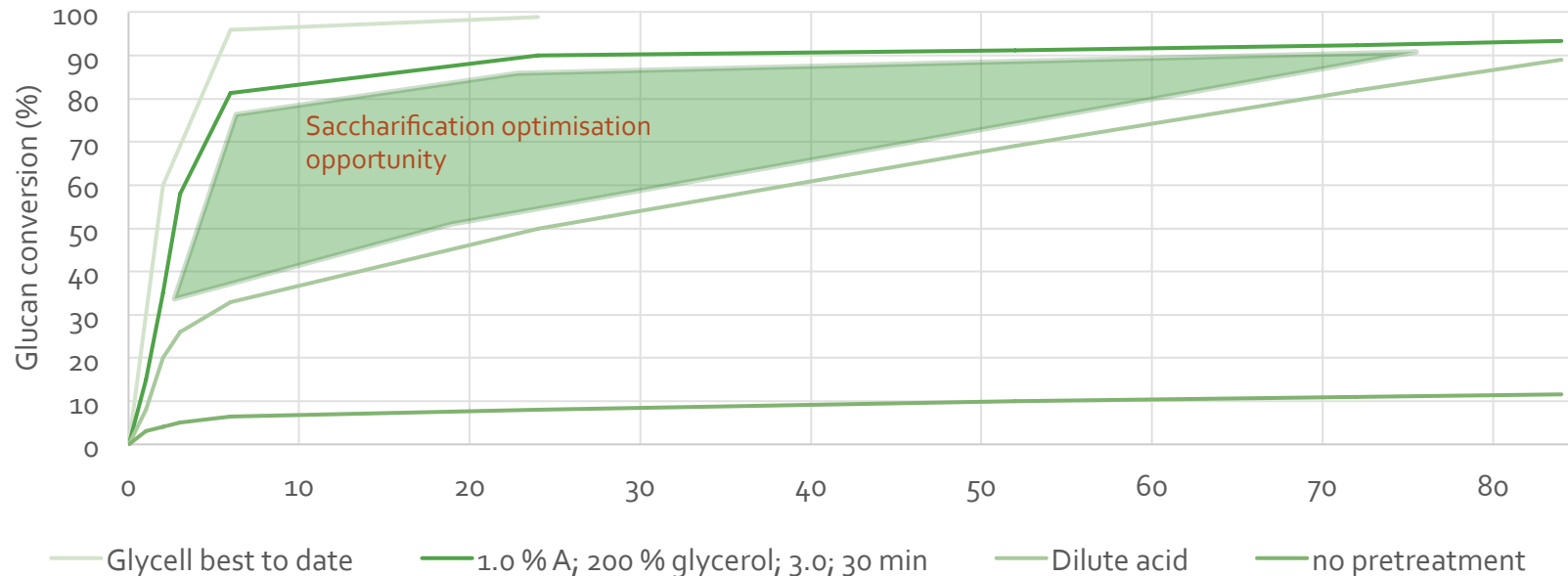


Andritz Pilot Plant, Springfield OH



Improved saccharification kinetics

Significant opportunity to reduce enzyme load and size of reactors

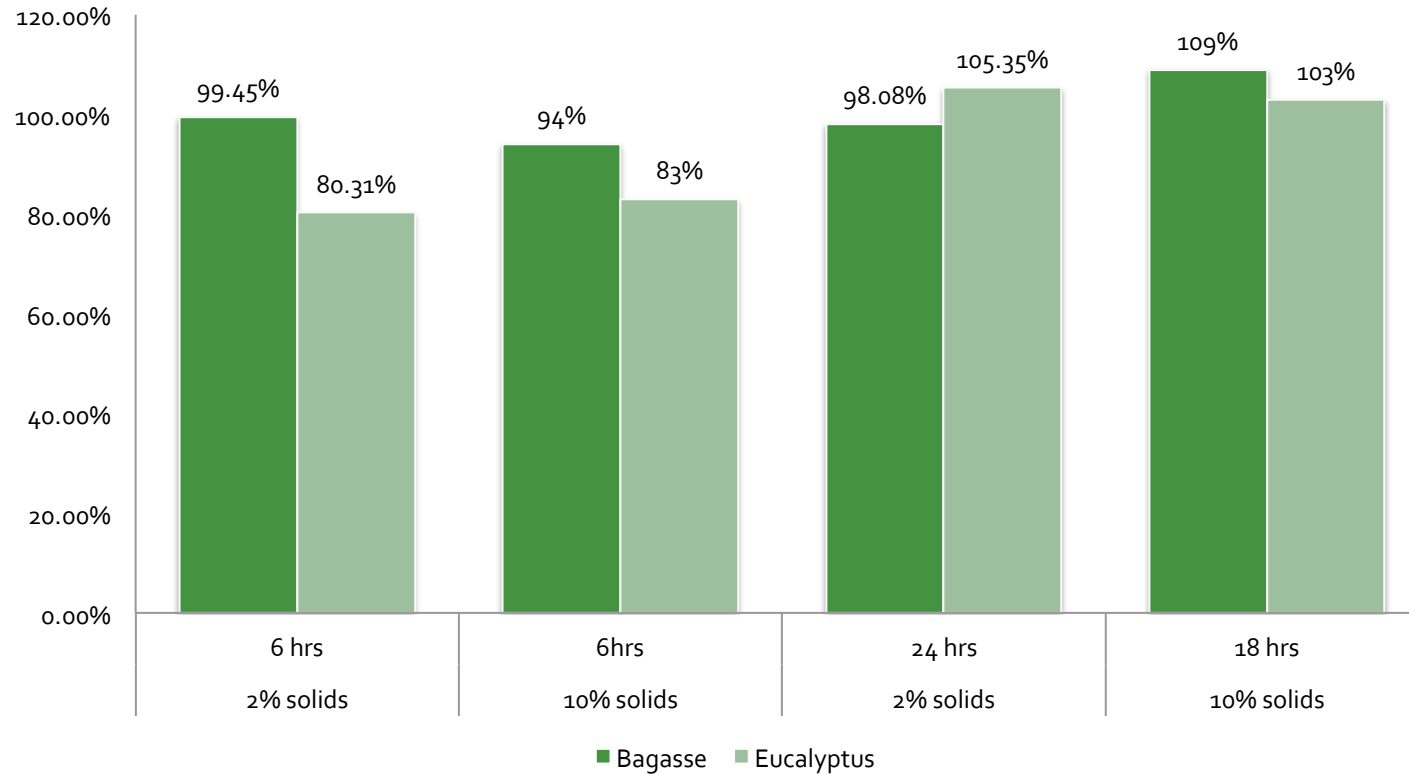


- ▶ Dilute acid – NREL design target (2013) – 0.9 % acid; 2.3 liquid:solid; 5 min – 90 % hydrolysis of cellulose after 84 hours with enzyme load of 10 mg/g cellulose
 - ▶ ca. 5 % conversion of xylan to furfural
- ▶ Glycell best to date – Hardwood – 0.8 % acid; 160 % glycerol; 2.4 liquid:solid; 30 min
 - ▶ No measurable furfural formation

Effects on solids loading on Glycell pretreated biomass

- ▶ pH 5.0 - 50°C optimal reaction temperature
- ▶ 2 & 10% solids
- ▶ 20 mg/g glucan enzyme dose tested
- ▶ Testing on Glycell bagasse and Eucalytus pretreated samples
- ▶ Confirmed washing effect

Enzymatic efficacy sustained at higher solids



- ▶ pH 5.0; 50 °C; 20 mg/g enzyme
- ▶ bagasse and eucalyptus at 2 and 10% solids

High solids saccharification



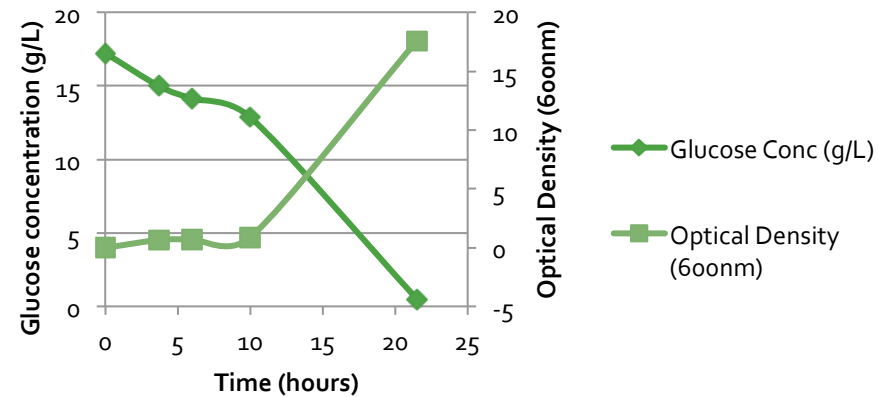
- ▶ High solids saccharification studies at Andritz (Glens Falls, NY)
- ▶ Glycell Pretreated poplar chips
 - ▶ Glycell - 1.15% acid on biomass db, 55% glycerol
 - ▶ Dilute acid - 1.07% acid on biomass db, no glycerol
- ▶ 15 % solids, pH 5.5, CTEC 3 at 12 mg/g of cellulose
- ▶ Initial cellulose saccharification rate of the Glycell pretreated biomass was 3.0 times that of dilute acid pretreatment.
- ▶ Final yield of monosaccharides from the Glycell pretreated biomass was 166.6% that of dilute acid pretreatment.

Fermentation testing - 2l biostats

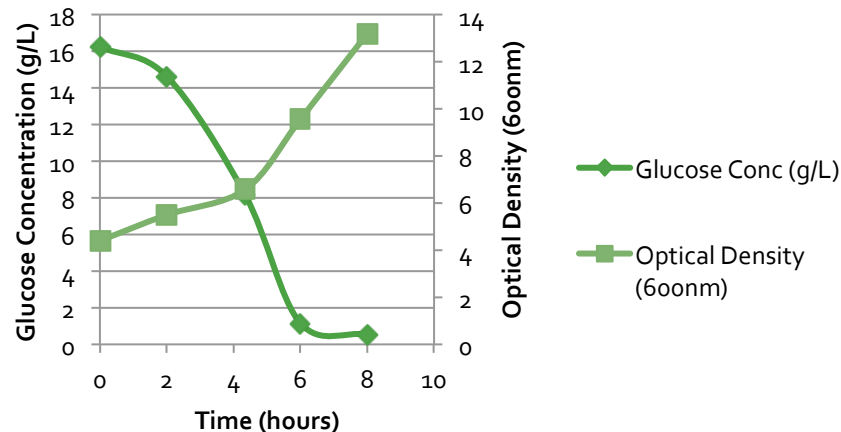
Sugars support microbial growth with no inhibition

	Ferment 1		Ferment 2		Ferment 3	
Organism	P. holstii		S. cerevisiae		E. coli	
Media (2L)	Tryptone	5g/L	Tryptone	5g/L	Tryptone	10g/L
	Yeast Extract	6g/L	Yeast Extract	6g/L	Yeast Extract	5g/L
	MgSO ₄ ·7H ₂ O	1g/L	MgSO ₄ ·7H ₂ O	1g/L	NaCl	10g/L
	KH ₂ PO ₄	5g/L	KH ₂ PO ₄	5g/L	Leaf Glucose Solution	44ml/L
	Leaf Glucose Solution	44ml/L	Leaf Glucose Solution	44ml/L	Antifoam C	1ml/L
	Antifoam C	1ml/L	Antifoam C	1ml/L		
pH	5.5		5.5		7.0	
Temperature	30°C		30°C		37°C	
Agitation	300rpm		300rpm		300rpm	
Air flow	4L/min		4L/min		4L/min	

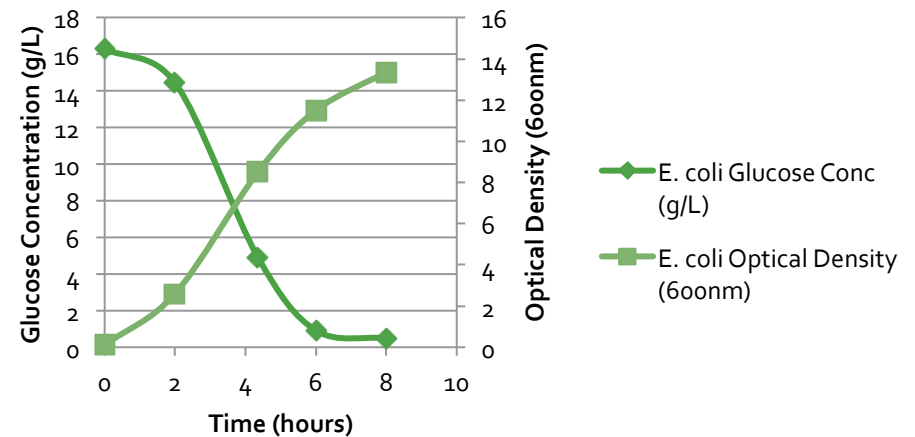
P. holstii



S. cerevisiae



E. coli

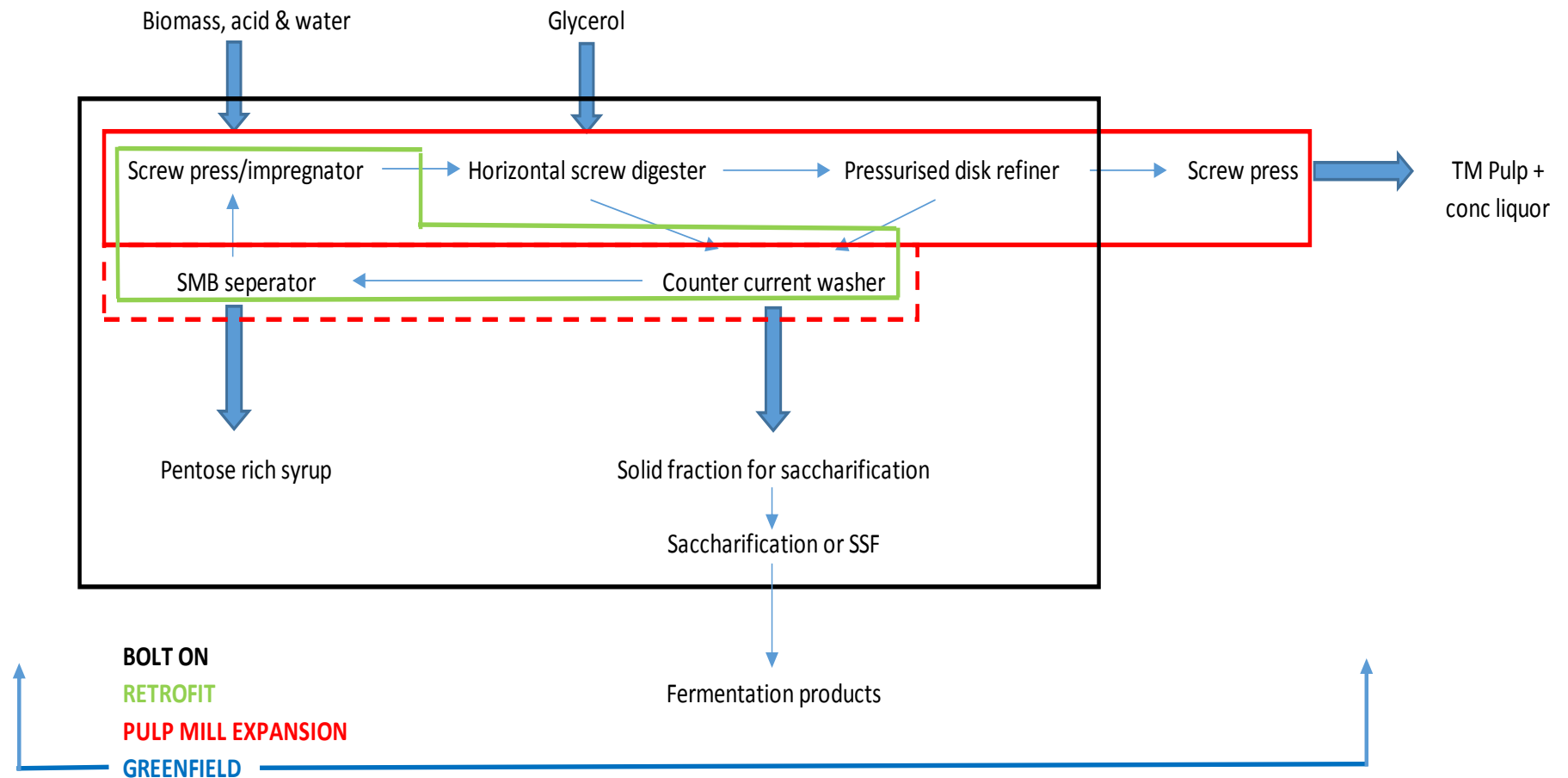


Glycerol recovery at Amalgamated Research LLC (ARi)

- ▶ ARi simulated moving bed chromatography services include:
 - ▶ Testing at the ARi pilot facility.
 - ▶ Lease of pilot skids for on-site testing.
 - ▶ Sale of custom design pilot plants for customer testing or demonstration purposes.
 - ▶ Project R&D, supervision and engineering from lab to industrial scale implementation.
- ▶ ARi testing on *ca.* 1 tonne of filtrate over 4 weeks confirms that >95% of the glycerol in the filtrate is recoverable by SMB chromatography at *ca.* 95% purity



Process modes for industry settings



Greenfield design case

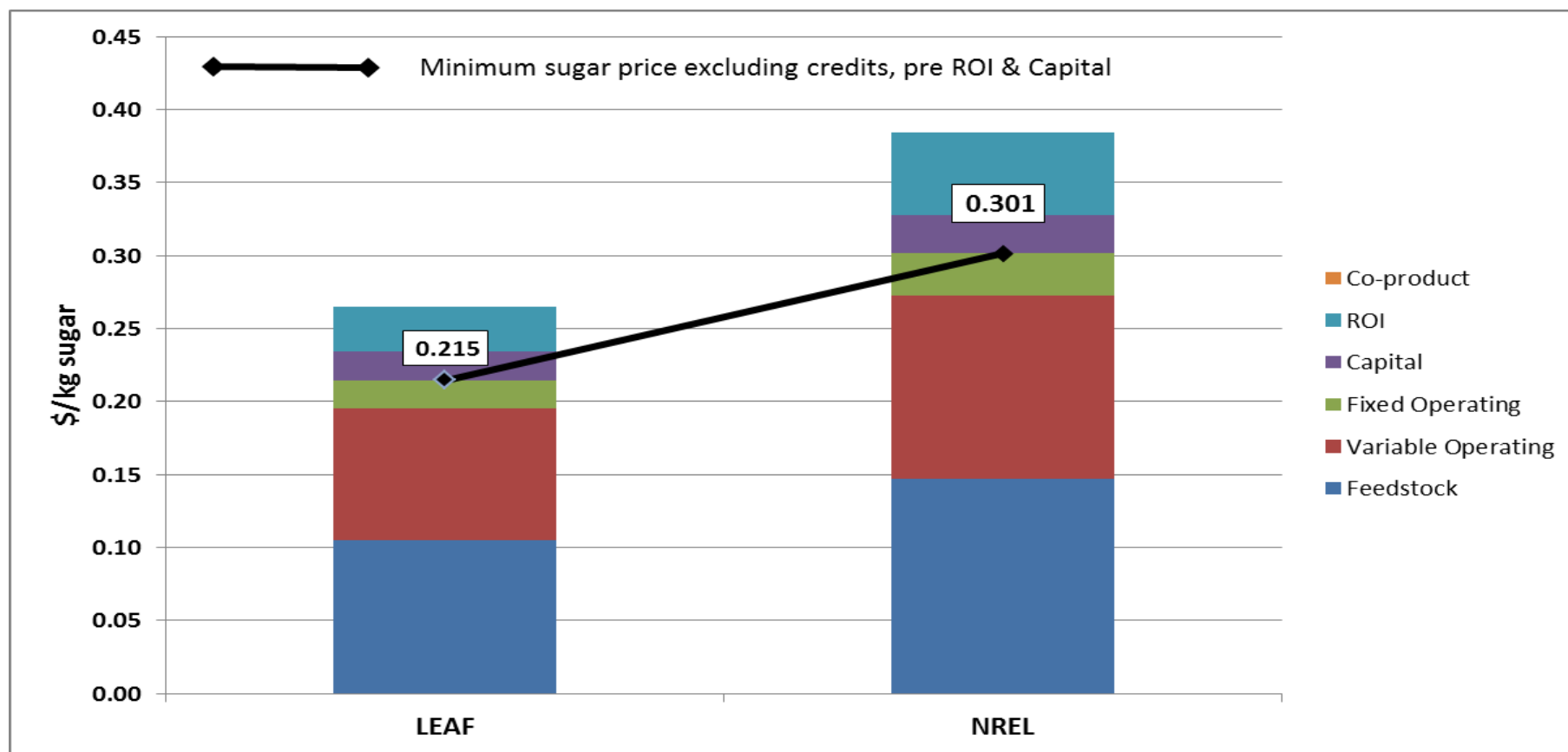
Glycell model vs Dilute acid model



- ▶ Common Class 5 estimate
 - ▶ 367,200 tonnes (d.b.) p.a. at \$66.10/dry tonne
 - ▶ 60% debt funding at 8% over 10 years
 - ▶ CapEx spend over 3 years and revenue commencing mid-year 3
- ▶ Dilute acid model (NREL design report)
 - ▶ Normalised to 80% cellulose to glucose efficiency
 - ▶ Capital required for enzyme production removed and purchase of enzymes included in OpEx

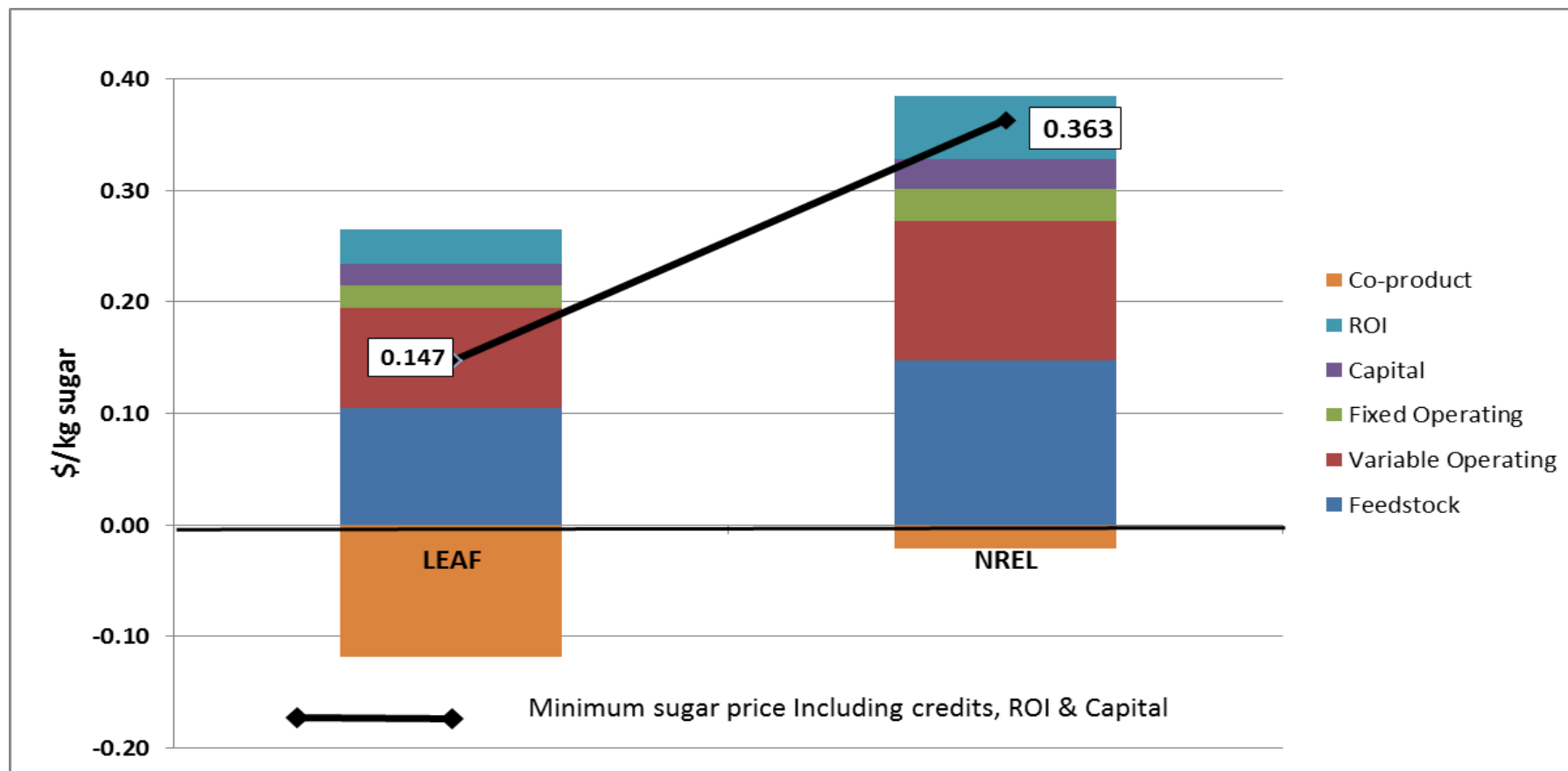


Greenfield design case – excluding coproduct benefit



- ▶ 28.7% advantage of Glycell over normalised NREL model (net of ROI and CapEx)
- ▶ Represents a \$0.09/kg saving

Greenfield design case – including coproduct benefit



- ▶ Includes CapEx and OpEx required to realise coproduct revenue (Glycell lignin at \$450/tonne)
- ▶ Represents a \$0.21/kg saving

Key competitive advantages



Based on current data, Leaf Energy's Glycell™ process when compared to other pretreatment processes, such as acid hydrolysis and/or steam explosion:

- ▶ Produces high yield cellulose with less degradation products.
- ▶ Improved enzymatic conversion of cellulose to sugars.
- ▶ Produces a high purity glucose liquor due to milder conditions and separation of pretreatment solids and liquids.
- ▶ Other possible benefits – glycerol pacifying metal surfaces impacts on cost and life of plant.

Thank You



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